

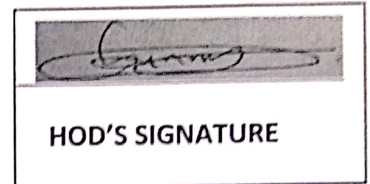


ELIZADE UNIVERSITY, ILARA-MOKIN,
ONDO STATE, NIGERIA
DEPARTMENT OF MECHANICAL ENGINEERING

SECOND SEMESTER EXAMINATIONS

2017/2018 ACADEMIC SESSION

COURSE: MEE302 – Thermodynamics
CLASS: 300 Level Mechanical & Automotive Engineering
TIME ALLOWED: 2 hours 30 minutes
INSTRUCTIONS: Attempt any four questions



Date: July/August, 2018

Question 1

- (a) Which is higher between the back work ratio of gas turbine and steam turbine engines? Explain **(5 marks)**
- (b) A gas-turbine power plant operating on an Ideal Brayton cycle has a pressure ratio, r_p , of 8. The gas temperature is 300 K at the compressor inlet and 1300 K at the turbine inlet. Utilizing the air-standard assumptions determine the gas temperature at the exits of (i) the compressor, (ii) the turbine (iii) the back work ratio, and (iv) the thermal efficiency **(10 marks)**

Question 2

- (a) Explain briefly the methods by which increase in the efficiency of a Rankine cycle can be achieved. **(6 marks)**
- (b) Consider a steam power plant operating on the simple ideal Rankine cycle. Steam enters the turbine at a 3 MPa and 350 °C and is condensed in the condenser at a pressure of 75 kPa. Determine the
- (i) thermal efficiency of this cycle.
(ii) back work ratio and
(iii) thermal efficiency of a Carnot cycle operating between the same limits **(9 marks)**

Question 3

- (a) Why is the Reversed Carnot cycle executed within the saturation dome not a realistic model for refrigeration cycle? **(6 marks)**
- (b) A refrigerator uses refrigerant-134a as the working fluid and operates on an ideal vapour-compression refrigeration cycle between 0.14 and 0.8 MPa. If the mass flow rate of the refrigerant is 0.05 kg/s, determine the
- rate of heat removal from the refrigerated space,
 - power input to the compressor,
 - rate of heat rejection to the environment, and the
 - COP of the refrigeration
- (9 marks)**

Question 4

- (a) Mention the **two critical factors** to be considered in refrigerant selection and any other **two factors** **(6 marks)**
- (b) A room $5\text{ m} \times 5\text{ m} \times 3\text{ m}$ contains air at $25\text{ }^\circ\text{C}$ and 100 kPa at a relative humidity of 75 percent. Take $c_p = 1.005\text{ kJ/kg}$, $R_a = 0.287\text{ kPa}\cdot\text{m}^3/\text{kg}\cdot\text{K}$, $R_v = 0.4615\text{ kPa}\cdot\text{m}^3/\text{kg}\cdot\text{K}$. Determine the
- partial pressure of dry air
 - specific humidity
 - enthalpy per unit mass of the dry air
 - masses of the dry air and water vapour in the room
- (9 marks)**

Question 5

- (a) On a hot afternoon, the outer surface of a glass of iced-water “sweats”. How can you explain this sweating? **(6 marks)**
- (b) A simple ideal Brayton cycle with air as the working fluid has a pressure ratio of 10. The air enters the compressor at 295 K and the turbine at 1240 K. Accounting for the variation of specific heats with temperature, determine the
- air temperature at the compressor exit,
 - back work ratio, and
 - thermal efficiency.
- (9 marks)**

Question 6

- (a) List **four** other types of refrigeration systems other than the vapour-compression refrigeration and mention **two refrigerants** **(6 marks)**
- (b) A gas-turbine power plant operating on an has a pressure ratio, r_p , of 8. The gas temperature is 300 K at the compressor inlet and 1300 K at the turbine inlet. Taking the compressor efficiency to be 80% and turbine efficiency to be 85% for the cycle, Determine the
- back work ratio
 - thermal efficiency
 - turbine exit temperature
- (9 marks)**

SELECTED RELEVANT FORMULAS

$$1. \frac{P_{r2}}{P_{r1}} = \frac{P_2}{P_1}$$

$$2. \eta_C = \frac{w_s}{w_a}$$

$$3. \eta_T = \frac{w_a}{w_s}$$

$$4. \eta_{th} = \frac{w_{net}}{q_{in}} \text{ or } \eta_{th} = 1 - \frac{q_{out}}{q_{in}}$$

$$5. (q_{in} - q_{out}) + (w_{in} - w_{out}) = h_e - h_i$$

$$6. w_{pump,in} = v(P_2 - P_1)$$

$$7. \dot{w} = \dot{m}(\Delta h)$$

$$8. \phi = \frac{P_v}{P_g}$$

$$9. \omega = \frac{0.622P_v}{P - P_v}$$

$$10. P = P_a + P_v$$

$$11. COP_R = \frac{Q_L}{W_{in}}$$

$$12. COP_{R,Carnot} = \frac{1}{(T_H/T_L)^{-1}}$$

TABLE A-17

Ideal-gas properties of air

T K	h kJ/kg	P _r	s kJ/kg	c _p	r kJ/kg·K	T K	h kJ/kg	P _r	s kJ/kg	c _p	r kJ/kg·K
290	290.16	1.2311	206.91	676.1	1.65802	680	691.82	25.85	496.62	75.50	2.54175
295	295.17	1.2048	210.89	647.9	1.68515	690	702.52	27.29	504.45	72.56	2.55731
298	298.18	1.2043	212.64	631.9	1.69528	700	713.27	28.80	512.33	69.76	2.57277
300	300.19	1.2060	214.07	621.2	1.70203	710	724.04	30.38	520.23	67.07	2.58810
305	305.22	1.1896	217.67	596.0	1.71865	720	734.82	32.02	528.14	64.50	2.60319
310	310.24	1.1646	221.25	572.3	1.73498	730	745.62	33.72	536.07	62.13	2.61803
315	315.27	1.1412	224.80	549.8	1.75106	740	756.44	35.50	544.02	59.82	2.63280
320	320.29	1.1191	228.42	528.4	1.76690	750	767.29	37.35	551.99	57.63	2.64737
325	325.31	1.1005	232.02	508.4	1.78249	760	778.18	39.27	560.01	55.54	2.66176
330	330.34	1.0852	235.61	489.4	1.79783	780	800.03	43.35	574.12	51.64	2.69013
340	340.42	1.049	242.82	454.1	1.82790	800	821.95	47.75	588.30	48.08	2.71787
350	350.49	1.0179	250.02	422.2	1.85708	820	843.98	52.59	608.59	44.84	2.74504
360	360.58	0.9906	257.24	393.4	1.88543	840	866.08	57.60	624.95	41.85	2.77170
370	370.67	0.9672	264.46	367.2	1.91313	860	888.27	63.09	641.40	39.12	2.79783
380	380.77	0.9476	271.69	343.4	1.94031	880	910.56	68.98	657.95	36.61	2.82344
390	390.88	0.9311	278.93	321.5	1.96693	900	932.93	75.29	674.58	34.31	2.84854
400	400.98	0.9174	286.16	301.6	1.99194	920	955.38	82.05	691.28	32.18	2.87324
410	411.12	0.9062	293.43	283.3	2.01639	940	977.92	89.28	708.08	30.22	2.89748
420	421.26	0.8972	300.69	266.6	2.04047	960	1000.55	97.00	725.02	28.40	2.92128
430	431.43	0.8901	307.99	251.1	2.06423	980	1023.25	105.2	741.98	26.73	2.94468
440	441.61	0.8847	315.30	236.8	2.08870	1000	1046.04	114.0	758.94	25.17	2.96770
450	451.80	0.8807	322.62	223.6	2.11161	1020	1068.89	123.4	776.10	23.72	2.99034
460	462.02	0.8780	329.97	211.4	2.13407	1040	1091.85	133.3	793.36	22.29	3.01260
470	472.24	0.8764	337.32	200.1	2.15604	1060	1114.86	143.9	810.62	21.14	3.03449
480	482.49	0.8758	344.70	189.5	2.17760	1080	1137.89	155.2	827.88	19.98	3.05608
490	492.74	0.8761	352.08	179.7	2.19876	1100	1161.07	167.1	845.33	18.896	3.07732
500	503.02	0.8774	359.49	170.6	2.21952	1120	1184.38	179.7	862.79	17.886	3.09825
510	513.32	0.8795	366.92	162.1	2.23993	1140	1207.87	193.1	880.35	16.946	3.11883
520	523.63	0.8824	374.36	154.1	2.25997	1160	1230.50	207.2	897.91	16.064	3.13914
530	533.98	0.8861	381.84	146.7	2.27967	1180	1254.34	222.2	915.57	15.241	3.15914
540	544.35	0.8906	389.34	139.7	2.29906	1200	1277.79	238.0	933.33	14.470	3.17888
550	554.74	0.8959	396.86	133.1	2.31809	1220	1301.31	254.7	951.09	13.747	3.19834
560	565.17	0.9020	404.42	127.0	2.33685	1240	1324.93	272.3	968.95	13.069	3.21751
570	575.63	0.9089	411.97	121.2	2.35531						

TABLE A-17

Ideal-gas properties of air

<i>T</i> K	<i>h</i> kJ/kg	<i>P_r</i>	<i>u</i> kJ/kg	<i>v_r</i>	<i>s^o</i> kJ/kg·K	<i>T</i> K	<i>h</i> kJ/kg	<i>P_r</i>	<i>u</i> kJ/kg	<i>v_r</i>	<i>s^o</i> kJ/kg·K
290	290.16	1.2311	206.91	676.1	1.66802	680	691.82	25.85	496.62	75.50	2.54175
295	295.17	1.3068	210.49	647.9	1.68515	690	702.52	27.29	504.45	72.56	2.55731
298	298.18	1.3543	212.64	631.9	1.69528	700	713.27	28.80	512.33	69.76	2.57277
300	300.19	1.3860	214.07	621.2	1.70203	710	724.04	30.38	520.23	67.07	2.58810
305	305.22	1.4686	217.67	596.0	1.71865	720	734.82	32.02	528.14	64.53	2.60319
310	310.24	1.5546	221.25	572.3	1.73498	730	745.62	33.72	536.07	62.13	2.61803
315	315.27	1.6442	224.85	549.8	1.75106	740	756.44	35.50	544.02	59.82	2.63280
320	320.29	1.7375	228.42	528.6	1.76690	750	767.29	37.35	551.99	57.63	2.64737
325	325.31	1.8345	232.02	508.4	1.78249	760	778.18	39.27	560.01	55.54	2.66176
330	330.34	1.9352	235.61	489.4	1.79783	780	800.03	43.35	576.12	51.64	2.69013
340	340.42	2.149	242.82	454.1	1.82790	800	821.95	47.75	592.30	48.08	2.71787
350	350.49	2.379	250.02	422.2	1.85708	820	843.98	52.59	608.59	44.84	2.74504
360	360.58	2.626	257.24	393.4	1.88543	840	866.08	57.60	624.95	41.85	2.77170
370	370.67	2.892	264.46	367.2	1.91313	860	888.27	63.09	641.40	39.12	2.79783
380	380.77	3.176	271.69	343.4	1.94001	880	910.56	68.98	657.95	36.61	2.82344
390	390.88	3.481	278.93	321.5	1.96633	900	932.93	75.29	674.58	34.31	2.84856
400	400.98	3.806	286.16	301.6	1.99194	920	955.38	82.05	691.28	32.18	2.87324
410	411.12	4.153	293.43	283.3	2.01699	940	977.92	89.28	708.08	30.22	2.89748
420	421.26	4.522	300.69	266.6	2.04142	960	1000.55	97.00	725.02	28.40	2.92128
430	431.43	4.915	307.99	251.1	2.06533	980	1023.25	105.2	741.98	26.73	2.94468
440	441.61	5.332	315.30	236.8	2.08870	1000	1046.04	114.0	758.94	25.17	2.96770
450	451.80	5.775	322.62	223.6	2.11161	1020	1068.89	123.4	776.10	23.72	2.99034
460	462.02	6.245	329.97	211.4	2.13407	1040	1091.85	133.3	793.36	23.29	3.01260
470	472.24	6.742	337.32	200.1	2.15604	1060	1114.86	143.9	810.62	21.14	3.03449
480	482.49	7.268	344.70	189.5	2.17760	1080	1137.89	155.2	827.88	19.98	3.05608
490	492.74	7.824	352.08	179.7	2.19876	1100	1161.07	167.1	845.33	18.896	3.07732
500	503.02	8.411	359.49	170.6	2.21952	1120	1184.28	179.7	862.79	17.886	3.09825
510	513.32	9.031	366.92	162.1	2.23993	1140	1207.57	193.1	880.35	16.946	3.11883
520	523.63	9.684	374.36	154.1	2.25997	1160	1230.92	207.2	897.91	16.064	3.13916
530	533.98	10.37	381.84	146.7	2.27967	1180	1254.34	222.2	915.57	15.241	3.15916
540	544.35	11.10	389.34	139.7	2.29906	1200	1277.79	238.0	933.33	14.470	3.17888
550	555.74	11.86	396.86	133.1	2.31809	1220	1301.31	254.7	951.09	13.747	3.19834
560	565.17	12.66	404.42	127.0	2.33685	1240	1324.93	272.3	968.95	13.069	3.21751
570	575.59	13.50	411.97	121.2	2.35531						

TABLE A-5

Saturated water—Pressure table

Press., <i>P</i> kPa	Sat. temp., <i>T</i> _{sat} °C	Specific volume, m ³ /kg		Internal energy, kJ/kg			Enthalpy, kJ/kg			Entropy, kJ/kg·K		
		Sat. liquid, <i>v</i> _f	Sat. vapor, <i>v</i> _g	Sat. liquid, <i>u</i> _f	Evap., <i>u</i> _{fg}	Sat. vapor, <i>u</i> _g	Sat. liquid, <i>h</i> _f	Evap., <i>h</i> _{fg}	Sat. vapor, <i>h</i> _g	Sat. liquid, <i>s</i> _f	Evap., <i>s</i> _{fg}	Sat. vapor, <i>s</i> _g
1.0	6.97	0.001000	129.19	29.302	2355.2	2384.5	29.303	2484.4	2513.7	0.1059	8.8690	8.9749
1.5	13.02	0.001001	87.964	54.686	2338.1	2392.8	54.688	2470.1	2524.7	0.1956	8.6314	8.8270
2.0	17.50	0.001001	66.990	73.431	2325.5	2398.9	73.433	2459.5	2532.9	0.2606	8.4621	8.7227
2.5	21.08	0.001002	54.242	88.422	2315.4	2403.8	88.424	2451.0	2539.4	0.3118	8.3302	8.6421
3.0	24.08	0.001003	45.654	100.98	2306.9	2407.9	100.98	2443.9	2544.8	0.3543	8.2222	8.5765
4.0	28.96	0.001004	34.791	121.39	2293.1	2414.5	121.39	2432.3	2553.7	0.4224	8.0510	8.4734
5.0	32.87	0.001005	28.185	137.75	2282.1	2419.8	137.75	2423.0	2560.7	0.4762	7.9176	8.3938
7.5	40.29	0.001008	19.233	168.74	2261.1	2429.8	168.75	2405.3	2574.0	0.5763	7.6738	8.2501
10	45.81	0.001010	14.670	191.79	2245.4	2437.2	191.81	2392.1	2583.9	0.6492	7.4996	8.1488
15	53.97	0.001014	10.020	225.93	2222.1	2448.0	225.94	2372.3	2598.3	0.7549	7.2522	8.0071
20	60.06	0.001017	7.6481	251.40	2204.6	2456.0	251.42	2357.5	2608.9	0.8320	7.0752	7.9073
25	64.96	0.001020	6.2034	271.93	2190.4	2462.4	271.96	2345.5	2617.5	0.8932	6.9370	7.8302
30	69.09	0.001022	5.2287	289.24	2178.5	2467.7	289.27	2335.3	2624.6	0.9441	6.8234	7.7675
40	75.86	0.001026	3.9933	317.58	2158.8	2476.3	317.62	2318.4	2636.1	1.0261	6.6430	7.6691
50	81.32	0.001030	3.2403	340.49	2142.7	2483.2	340.54	2304.7	2645.2	1.0912	6.5019	7.5931
75	91.76	0.001037	2.2172	384.36	2111.8	2496.1	384.44	2278.0	2662.4	1.2132	6.2426	7.4558
100	99.61	0.001043	1.6941	417.40	2088.2	2505.6	417.51	2257.5	2675.0	1.3028	6.0562	7.3589
101.325	99.97	0.001043	1.6734	418.95	2087.0	2506.0	419.06	2256.5	2675.6	1.3069	6.0476	7.3545
125	105.97	0.001048	1.3750	444.23	2068.8	2513.0	444.36	2240.6	2684.9	1.3741	5.9100	7.2841
150	111.35	0.001053	1.1594	466.97	2052.3	2519.2	467.13	2226.0	2693.1	1.4337	5.7894	7.2231
175	116.04	0.001057	1.0037	486.82	2037.7	2524.5	487.01	2213.1	2700.2	1.4850	5.6865	7.1716
200	120.21	0.001061	0.88578	504.50	2024.6	2529.1	504.71	2201.6	2706.3	1.5302	5.5968	7.1270
225	123.97	0.001064	0.79329	520.47	2012.7	2533.2	520.71	2191.0	2711.7	1.5706	5.5171	7.0877
250	127.41	0.001067	0.71873	535.08	2001.8	2536.8	535.35	2181.2	2716.5	1.6072	5.4453	7.0525
275	130.58	0.001070	0.65732	548.57	1991.6	2540.1	548.86	2172.0	2720.9	1.6408	5.3800	7.0207
300	133.52	0.001073	0.60582	561.11	1982.1	2543.2	561.43	2163.5	2724.9	1.6717	5.3200	6.9917
325	136.27	0.001076	0.56199	572.84	1973.1	2545.9	573.19	2155.4	2728.6	1.7005	5.2645	6.9650
350	138.86	0.001079	0.52422	583.89	1964.6	2548.5	584.26	2147.7	2732.0	1.7274	5.2128	6.9402
375	141.30	0.001081	0.49133	594.32	1956.6	2550.9	594.73	2140.4	2735.1	1.7526	5.1645	6.9171
400	143.61	0.001084	0.46242	604.22	1948.9	2553.1	604.66	2133.4	2738.1	1.7765	5.1191	6.8955

TABLE A-6

Superheated water (Concluded)

<i>T</i> °C	<i>P</i> = 2.50 MPa (223.95°C)				<i>P</i> = 3.00 MPa (233.85°C)			
	<i>v</i> m ³ /kg	<i>u</i> kJ/kg	<i>h</i> kJ/kg	<i>s</i> kJ/kg·K	<i>v</i> m ³ /kg	<i>u</i> kJ/kg	<i>h</i> kJ/kg	<i>s</i> kJ/kg·K
Sat.	0.07995	2602.1	2801.9	6.2558	0.06667	2603.2	2803.2	6.1856
225	0.08026	2604.8	2805.5	6.2629				
250	0.08705	2663.3	2880.9	6.4107	0.07063	2644.7	2856.5	6.2893
300	0.09894	2762.2	3009.6	6.6459	0.08118	2750.8	2994.3	6.5412
350	0.10979	2852.5	3127.0	6.8424	0.09056	2844.4	3116.1	6.7450
400	0.12012	2939.8	3240.1	7.0170	0.09938	2933.6	3231.7	6.9235
450	0.13015	3026.2	3351.6	7.1768	0.10789	3021.2	3344.9	7.0856
500	0.13999	3112.8	3462.8	7.3254	0.11620	3108.6	3457.2	7.2359
600	0.15931	3288.5	3686.8	7.5979	0.13245	3285.5	3682.8	7.5103
700	0.17835	3469.3	3915.2	7.8455	0.14841	3467.0	3912.2	7.7590
800	0.19722	3656.2	4149.2	8.0744	0.16420	3654.3	4146.9	7.9885
900	0.21597	3849.4	4389.3	8.2882	0.17988	3847.9	4387.5	8.2028
1000	0.23466	4049.0	4635.6	8.4897	0.19549	4047.7	4634.2	8.4045
1100	0.25330	4254.7	4887.9	8.6804	0.21105	4253.6	4886.7	8.5955
1200	0.27190	4466.3	5146.0	8.8618	0.22658	4465.3	5145.1	8.7771
1300	0.29048	4683.4	5409.5	9.0349	0.24207	4682.6	5408.8	8.9502

Saturated refrigerant-134a—Pressure table

Press., <i>P</i> kPa	Sat. temp., <i>T</i> _{sat} °C	Specific volume, m ³ /kg		Internal energy, kJ/kg			Enthalpy, kJ/kg			Entropy, kJ/kg·K		
		Sat. liquid, <i>v</i> _f	Sat. vapor, <i>v</i> _g	Sat. liquid, <i>u</i> _f	Evap., <i>u</i> _{fg}	Sat. vapor, <i>u</i> _g	Sat. liquid, <i>h</i> _f	Evap., <i>h</i> _{fg}	Sat. vapor, <i>h</i> _g	Sat. liquid, <i>s</i> _f	Evap., <i>s</i> _{fg}	Sat. vapor, <i>s</i> _g
120	-22.32	0.0007324	0.16212	22.40	195.11	217.51	22.49	214.48	236.97	0.09275	0.85503	0.94779
140	-18.77	0.0007383	0.14014	26.98	192.57	219.54	27.08	212.08	239.16	0.11087	0.83368	0.94456
160	-15.60	0.0007437	0.12348	31.09	190.27	221.35	31.21	209.90	241.11	0.12693	0.81496	0.94190
180	-12.73	0.0007487	0.11041	34.83	188.16	222.99	34.97	207.90	242.86	0.14139	0.79826	0.93965
200	-10.09	0.0007533	0.099867	38.28	186.21	224.48	38.43	206.03	244.46	0.15457	0.78316	0.93773
700	26.69	0.0008331	0.029361	88.24	156.24	244.48	88.82	176.21	265.03	0.33230	0.58763	0.91994
750	29.06	0.0008395	0.027371	91.59	154.08	245.67	92.22	173.98	266.20	0.34345	0.57567	0.91912
800	31.31	0.0008458	0.025621	94.79	152.00	246.79	95.47	171.82	267.29	0.35404	0.56431	0.91835
850	33.45	0.0008520	0.024069	97.87	149.98	247.85	98.60	169.71	268.31	0.36413	0.55349	0.91762
900	35.51	0.0008580	0.022683	100.83	148.01	248.85	101.61	167.66	269.26	0.37377	0.54315	0.91692
950	37.48	0.0008641	0.021438	103.69	146.10	249.79	104.51	165.64	270.15	0.38301	0.53323	0.91624

Superheated refrigerant-134a (Continued)

<i>T</i> °C	<i>v</i> m ³ /kg	<i>u</i> kJ/kg	<i>h</i> kJ/kg	<i>s</i> kJ/kg·K	<i>v</i> m ³ /kg	<i>u</i> kJ/kg	<i>h</i> kJ/kg	<i>s</i> kJ/kg·K	<i>v</i> m ³ /kg	<i>u</i> kJ/kg	<i>h</i> kJ/kg	<i>s</i> kJ/kg·K
<i>P</i> = 0.80 MPa (<i>T</i> _{sat} = 31.31°C)				<i>P</i> = 0.90 MPa (<i>T</i> _{sat} = 35.51°C)				<i>P</i> = 1.00 MPa (<i>T</i> _{sat} = 39.37°C)				
Sat.	0.025621	246.79	267.29	0.9183	0.022683	248.85	269.26	0.9169	0.020313	250.68	270.99	0.9156
40	0.027035	254.82	276.45	0.9480	0.023375	253.13	274.17	0.9327	0.020406	251.30	271.71	0.9179
50	0.028547	263.86	286.69	0.9802	0.024809	262.44	284.77	0.9660	0.021796	260.94	282.74	0.9525
60	0.029973	272.83	296.81	1.0110	0.026146	271.60	295.13	0.9976	0.023068	270.32	293.38	0.9850

Saturated water—Temperature table

Temp., <i>T</i> °C	Sat. press., <i>P</i> _{sat} kPa	Specific volume, m ³ /kg		Internal energy, kJ/kg			Enthalpy, kJ/kg			Entropy, kJ/kg·K		
		Sat. liquid, <i>v</i> _f	Sat. vapor, <i>v</i> _g	Sat. liquid, <i>u</i> _f	Evap., <i>u</i> _{fg}	Sat. vapor, <i>u</i> _g	Sat. liquid, <i>h</i> _f	Evap., <i>h</i> _{fg}	Sat. vapor, <i>h</i> _g	Sat. liquid, <i>s</i> _f	Evap., <i>s</i> _{fg}	Sat. vapor, <i>s</i> _g
0.01	0.6117	0.001000	206.00	0.000	2374.9	2374.9	0.001	2500.9	2500.9	0.0000	9.1556	9.1556
5	0.8725	0.001000	147.03	21.019	2360.8	2381.8	21.020	2489.1	2510.1	0.0763	8.9487	9.0249
10	1.2281	0.001000	106.32	42.020	2346.6	2388.7	42.022	2477.2	2519.2	0.1511	8.7488	8.8999
15	1.7057	0.001001	77.885	62.980	2332.5	2395.5	62.982	2465.4	2528.3	0.2245	8.5559	8.7803
20	2.3392	0.001002	57.762	83.913	2318.4	2402.3	83.915	2453.5	2537.4	0.2965	8.3696	8.6661
25	3.1698	0.001003	43.340	104.83	2304.3	2409.1	104.83	2441.7	2546.5	0.3672	8.1895	8.5567
30	4.2469	0.001004	32.879	125.73	2290.2	2415.9	125.74	2429.8	2555.6	0.4368	8.0152	8.4520